

NEW PATENT APPLICATION COVER PAGE

**TITLE: HETEROCYCLIC-AMIDE CATALYST COMPOSITIONS FOR THE
POLYMERIZATION OF OLEFINS**

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**INVENTORS: Rex E. Murray
5921 Dalewood Drive
Apt. 522
Cross Lanes, WV 25313
Citizenship: United States of America**

**CORRESPONDENCE ADDRESS: Lisa Kimes Jones
Univation Technologies, LLC
5555 San Felipe, Suite 1950
Houston, TX 77056**

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HETEROCYCLIC-AMIDE CATALYST COMPOSITIONS FOR THE POLYMERIZATION OF OLEFINS

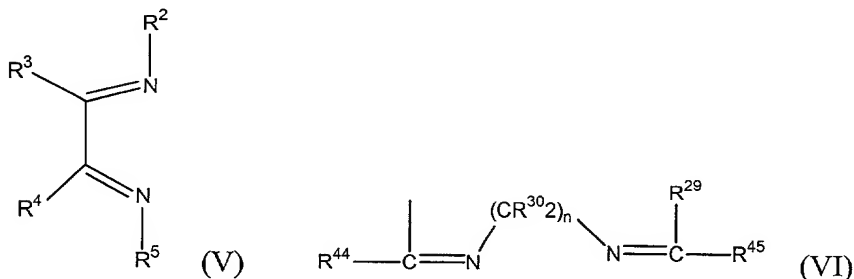
FIELD OF THE INVENTION

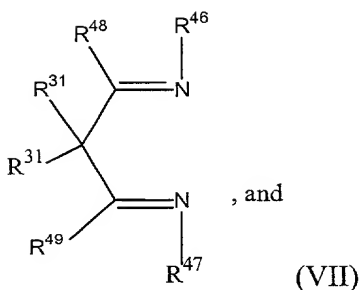
[0001] The present invention relates to a family of novel heterocyclic-amide type catalyst precursors useful for the polymerization of olefins, such as ethylene, higher alpha-olefins, dienes, or other monomers and mixtures thereof.

BACKGROUND OF THE INVENTION

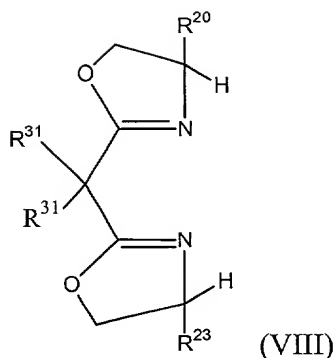
[0002] A variety of metallocenes and other single site-like catalysts have been developed to prepare olefin polymers. Metallocenes are organometallic coordination complexes containing one or more pi-bonded moieties (i.e., cyclopentadienyl groups) in association with a metal atom. Catalyst compositions containing metallocenes and other single site-like catalysts are highly useful for the preparation of polyolefins, producing relatively homogeneous copolymers at excellent polymerization rates while allowing one to closely tailor the final properties of the polymer as desired.

[0003] Recently, work relating to certain nitrogen-containing, single site-like catalyst precursors has been published. For example, PCT application No. WO 96/23101 relates to di(imine) metal complexes that are transition metal complexes of bidentate ligands selected from the group consisting of:





, and



wherein said transition metal is selected from the group consisting of Ti, Zr, Sc, V, Cr, a rare earth metal, Fe, Co, Ni, and Pd;

R^2 and R^5 are each independently hydrocarbyl or substituted hydrocarbyl, provided that the carbon atom bound to the imino nitrogen atom has at least two carbon atoms bound to it;

R^3 and R^4 are each independently, hydrogen, hydrocarbyl, substituted hydrocarbyl, or R^3 and R^4 taken together are hydrocarbylene or substituted hydrocarbylene to form a carbocyclic ring;

R^{44} is a hydrocarbyl or substituted hydrocarbyl, and R^{28} is hydrogen, hydrocarbyl or substituted hydrocarbyl or R^{44} and R^{28} taken together form a ring;

R^{45} is a hydrocarbyl or substituted hydrocarbyl, and R^{29} is hydrogen, hydrocarbyl or substituted hydrocarbyl or R^{45} and R^{29} taken together form a ring;

each R^{30} is independently hydrogen, hydrocarbyl or substituted hydrocarbyl, or two of R^{30} taken together form a ring;

each R^{31} is independently hydrogen, hydrocarbyl or substituted hydrocarbyl;

R^{46} and R^{47} are each independently hydrocarbyl or substituted hydrocarbyl, provided that the carbon atom bound to the imino nitrogen atom has at least two carbon atoms bound to it;

R^{48} and R^{49} are each independently hydrogen, hydrocarbyl, or substituted hydrocarbyl;

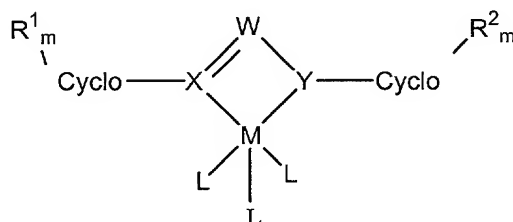
R^{20} and R^{23} are each independently hydrocarbyl, or substituted hydrocarbyl;

R^{21} and R^{22} are independently hydrogen, hydrocarbyl, or substituted hydrocarbyl; and

the transition metal also has bonded to it a ligand that may be displaced by or added to the olefin monomer being polymerized; and

when the transition metal is Pd, said bidentate ligand is (V), (VII) or (VIII).

[0004] Also, U.S. Patent No. 6,096,676, which is incorporated herein by reference, teaches a catalyst precursor having the formula:



each L is a monovalent, bivalent, or trivalent anion;

each cyclo is a cyclic moiety;

each R¹ is a group containing 1 to 50 atoms selected from the group consisting of hydrogen and Group IIIA to Group VIIA elements, and two or more adjacent R¹ groups may be joined to form a cyclic moiety;

each R² is a group containing 1 to 50 atoms selected from the group consisting of hydrogen and Group IIIA to Group VIIA elements and two or more adjacent R² groups may be joined to form a cyclic moiety;

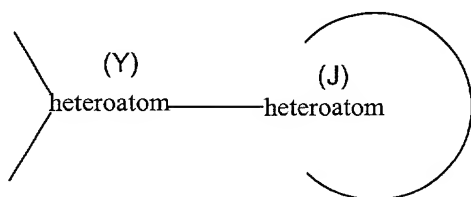
each m is independently an integer from 0 to 5.

[0005] Also taught is a catalyst composition comprising this catalyst precursor and an activating co-catalyst, as well as a process for the polymerization of olefins using this catalyst composition.

[0006] Although there are a variety of single site catalysts taught in the prior art, some of which are commercially available, there still exist a need in the art for improved catalysts and catalyst precursors that are capable of producing polyolefins having predetermined properties.

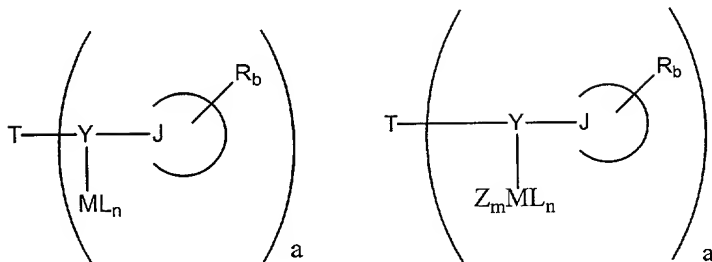
SUMMARY OF THE INVENTION

[0007] In accordance with the present invention there is provided catalyst precursors that contain the grouping:



wherein one heteroatom (J) is part of a ring structure and the other (X) is not. The most preferred heteroatom catalyst precursors are those wherein the heteroatom-containing ring moiety is a pyrrole or a piperidine and wherein the non-ring structure heteroatom moiety is an amide or amido group when Y is nitrogen and a phosphide or phosphido group when Y is phosphorus.

[0008] The catalyst precursors of the present invention can be represented by a formula selected from the following Group A formulae, Group B formulae, or Group C formulae.

Group A Formulae

where a is an integer from 1 to 5;

T is a chemical moiety having one or more, preferably 1 to 100 atoms, which can include hydrogen when a = 1, and T is a bridging group that bridges the Y atoms when a = 2 to 5;

M is a metallic element selected from Groups 1 to 15, and the Lanthanide series of the Periodic Table of the Elements;

Z is a coordination ligand;

m is an integer from 1 to 3;

each L is a monovalent, bivalent, or trivalent anionic ligand;

n is an integer from 1 to 6;

m is an integer from 0 to 5;

Y is a heteroatom selected from nitrogen, oxygen, sulfur, and phosphorus;

J is a heteroatom that is part of a ring structure and is selected from nitrogen, oxygen, sulfur, and phosphorus;

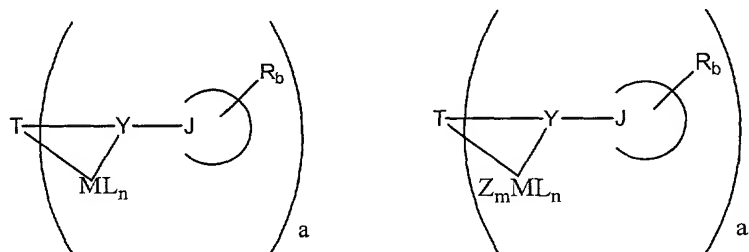
R can be independently hydrogen, or a non-bulky or a bulky substituent. If it is independently a non-bulky substituent it will have relatively low steric hindrance with respect to Y, and it is preferably a C₁ to C₂₀ alkyl group, preferably a primary alkyl group. Low steric hindrance, as used herein means that the non-bulky R group has no branching within 3 atoms of Y.

If R is independently a bulky group it will have a relatively large steric hindrance with respect to Y, and it will preferably be selected from alkyl (preferably branched), alkenyl (preferably branched), cycloalkyl, heterocyclic (both heteroalkyl and heteroaryl), aryl, alkylaryl, arylalkyl, and polymeric, including metallorganics such as

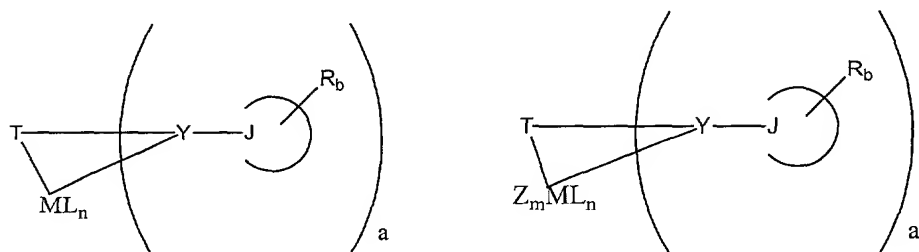
the P-N ring structures set forth below and inorganic-organic hybrid structures, also such as those set forth below. It is preferred that R, when bulky, contain from about 3 to 50, more preferably from about 3 to 30 non-hydrogen atoms, and most preferably from about 2 to 20 atoms. Also, one or more of the carbon or hydrogen positions can be substituted with an element other than carbon and hydrogen, preferably an element selected from Groups 14 to 17, more preferably a Group 14 element such as silicon, a Group 15 element such as nitrogen, a Group 16 element such as oxygen, or a Group 17 halogen.

b is an integer from 0 to 20.

Group B Formulae



Group C Formulae



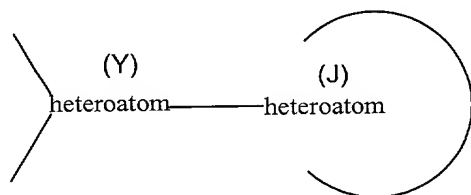
where T is a bridging group containing one or more bridging atoms and wherein Y, M, L, Z, R, b, n, m, and a are as defined above for the Group A formulae.

BRIEF DESCRIPTION OF THE FIGURE

[0009] The sole figure hereof shows two plots of molecular weight distribution as a function of the log of molecular weight, as measured by size exclusion chromatography, using the amine derived from the alkylation of 2-acetylpyridine(1-amino-cis-2,6-dimethyl piperidine)imine with tetrabenzyl zirconium. One plot represents the catalyst containing 0.5 micromoles of Zr and the other represents the catalyst containing 2.0 micromoles of Zr.

DETAILED DESCRIPTION OF THE INVENTION

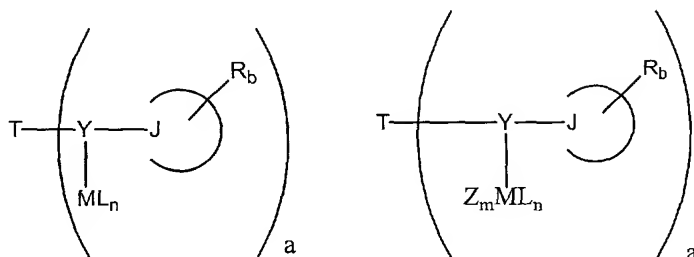
[0010] As previously mentioned the present invention relates to catalyst precursors that contain the grouping:



wherein one heteroatom (J) is part of a ring structure and the other (Y) is not. As mentioned above, the most preferred heteroatom catalyst precursors are those wherein the heteroatom-containing ring moiety is a pyrrole or a piperidine and wherein the non-ring structure heteroatom moiety is an amide or amido group when Y is nitrogen and a phosphide or phosphido group when Y is phosphorus.

[0011] The catalyst precursors of the present invention can be any of those represented by any of the following formulae.

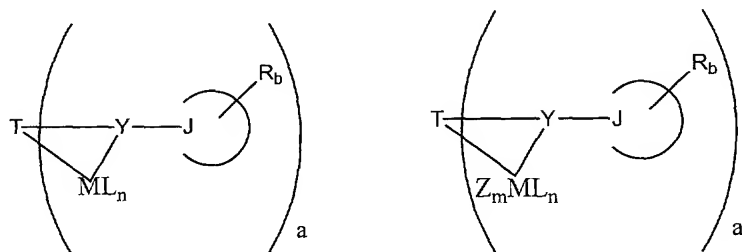
Group A Formulae

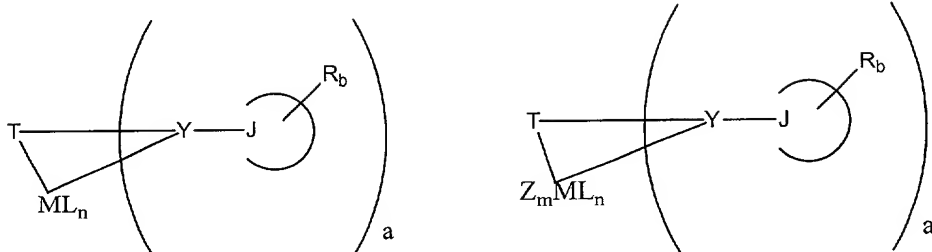


wherein a is an integer from 1 to 5;

T is a chemical moiety having one or more, preferably 1 to 100 atoms, which can include hydrogen when a = 1, and T is a bridging group that bridges the Y atoms when a = 2 to 5;

Group B Formulae



Group C Formulae

wherein for the Group B and Group C formulae T is a bridging moiety for bridging Y and M.

[0012] M is a metallic element selected from Groups 1 to 15, preferably from Groups 3 to 13 elements, more preferably the transition metals from Groups 3 to 7, and the Lanthanide series of the Periodic Table of the Elements. The Periodic Table of the Elements referred to herein is that table that appears in the inside front cover of Lange's Handbook of Chemistry, 15th Edition, 1999, McGraw Hill Handbooks.

[0013] Z is a coordination ligand. Preferred coordination ligands include triphenylphosphine, tris(C₁-C₆ alkyl) phosphine, tricycloalkyl phosphine, diphenyl alkyl phosphine, dialkyl phenyl phosphine, trialkylamine, arylamine such as pyridine, substituted or unsubstituted C₂ to C₂₀ alkenes (e.g. ethylene, propylene, butene, hexane, octane, decene, dodecene, allyl, and the like) in which the substituent is a halogen atom (preferably chloro), an ester group, a C₁ to C₄ alkoxy group, an amine group (-NR₂ where each R individually is a C₁ to C₃ alkyl), carboxylic acid, alkali metal salt, di(C₁ to C₄) alkyl ether, tetrahydrofuran (THF), a nitrile such as acetonitrile, an η⁴-diene, and the like.

[0014] Each L is a monovalent, bivalent, or trivalent anionic ligand, preferably containing from about 1 to 50 non-hydrogen atoms, more preferably from about 1 to 20 non-hydrogen atoms and is independently selected from the group consisting of

halogen containing groups; hydrogen; alkyl; aryl; alkenyl; alkylaryl; arylalkyl; hydrocarboxy; amides, phosphides; sulfides; silyalkyls; diketones; borohydrides; and carboxylates. More preferred are alkyl, arylalkyl, and halogen containing groups.

[0015] n is an integer from 1 to 6, preferably from 1 to 4, more preferably from 1 to 3.

[0016] Y is a heteroatom selected from nitrogen, oxygen, sulfur, and phosphorus, preferably selected from nitrogen and phosphorus, and more preferably nitrogen.

[0017] J is a heteroatom that is part of a ring structure, which heteroatom is selected from the group consisting of nitrogen, oxygen, sulfur, and phosphorus; preferably nitrogen and phosphorus, and more preferably nitrogen.

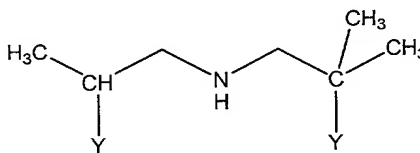
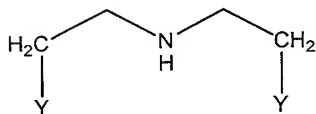
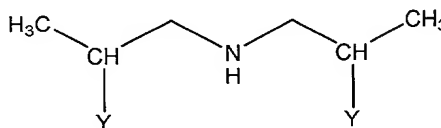
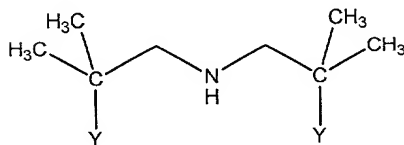
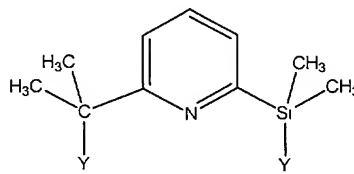
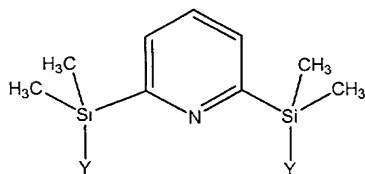
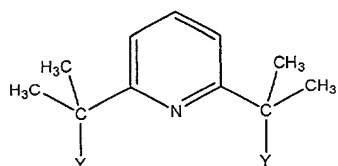
[0018] It is preferred that the ring be a five or six member ring, more preferably a pyrrole or a piperidine ring structure.

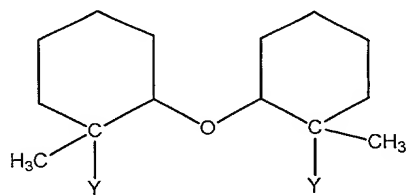
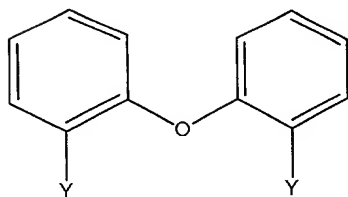
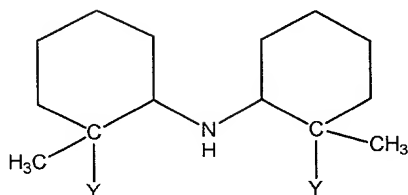
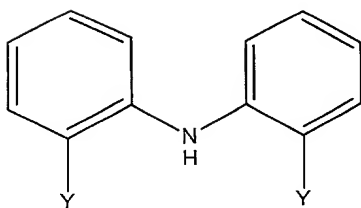
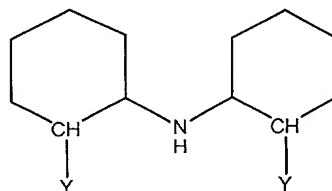
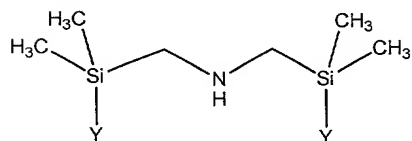
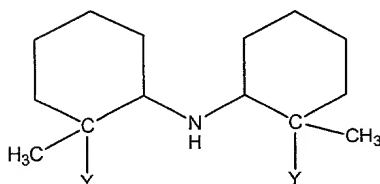
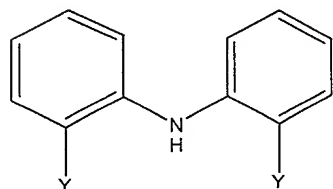
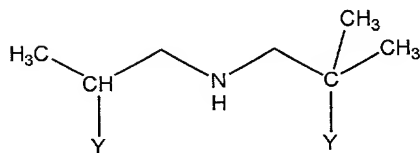
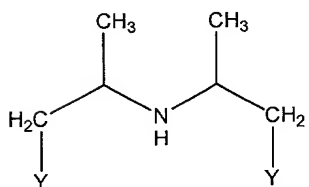
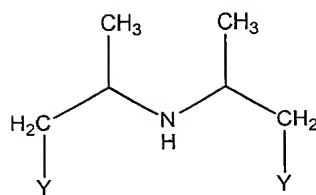
[0019] R can be a non-bulky substituent or a bulky substituent. By a non-bulky substituent we mean that it has relatively low steric hindrance with respect to Y. Non-limiting examples of non-bulky substituents include straight and branched chain alkyl groups, preferably straight chain groups. R is also preferably a C₁ to C₃₀ alkyl group, more preferably a C₁ to C₂₀ alkyl group, and most preferably an n-octyl group. If the non-bulky group is branched, the branch point must be at least 3 atoms removed from Y.

[0020] R can also be a bulky substituent. By bulky substituent we mean that R will be sterically hindering with respect to Y. When R is a bulky substituent it can be selected from alkyl, alkenyl, cycloalkyl, heterocyclic (both heteroalkyl and heteroaryl), alkylaryl, arylalkyl, and polymeric, including inorganics such as the P-N ring structures set forth below and inorganic-organic hybrid structures, such as those

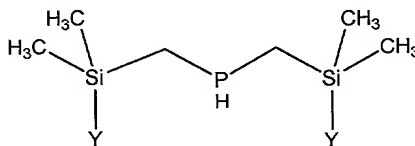
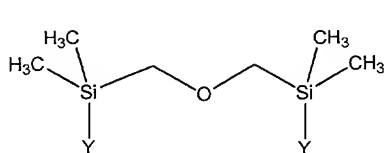
set forth below. It is preferred that the R substituent contain from about 1 to 50, more preferably from about 1 to 20 non-hydrogen atoms. Also, one or more of the carbon or hydrogen positions may be substituted with an element other than carbon and hydrogen, preferably an element selected from Groups 14 to 17, more preferably a Group 14 element such as silicon, a Group 15 element such as nitrogen, a Group 16 element such as oxygen, or a Group 17 halogen.

[0021] When $a = 2$, that is when there are two Y atoms, preferred T groups that can be used for Group C formulae compositions are selected from:

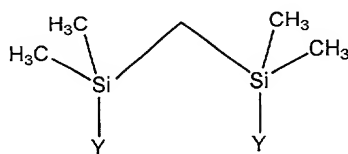
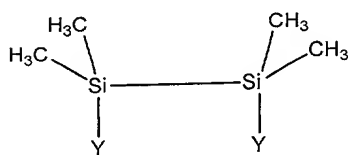




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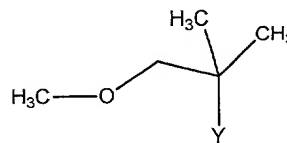
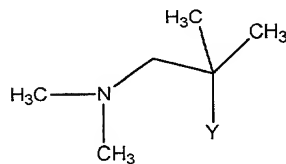
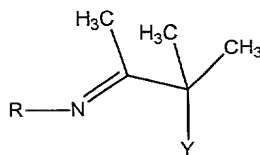
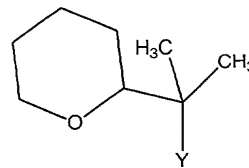
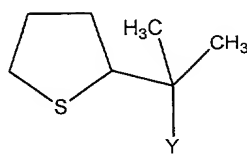
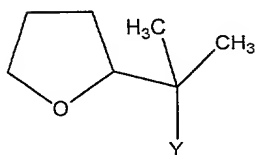
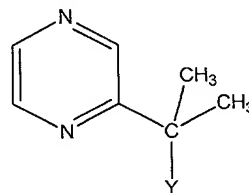
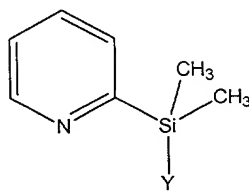
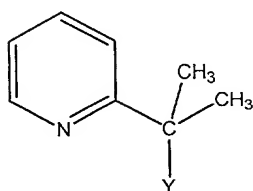


[0022] The following T groups can also be used when $a=2$, for compositions represented by Group A formulae:

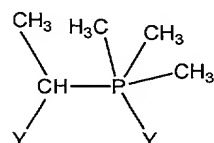
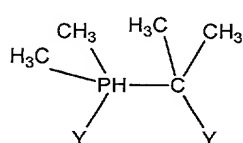
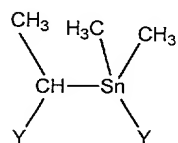
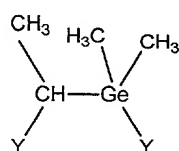
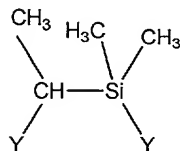
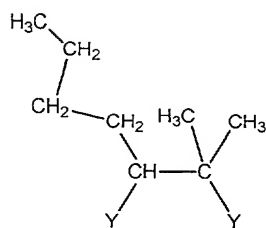
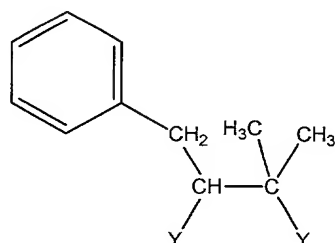
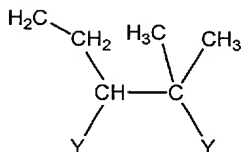
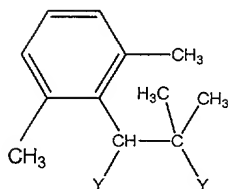
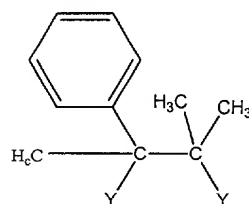
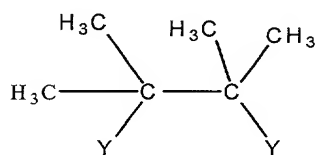
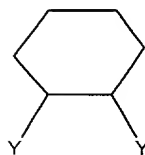
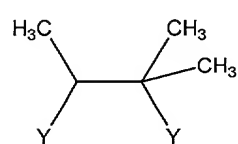
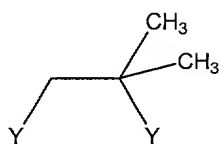
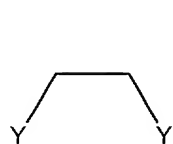


wherein the Y atoms are provided for convenience and are not part of the T moiety.

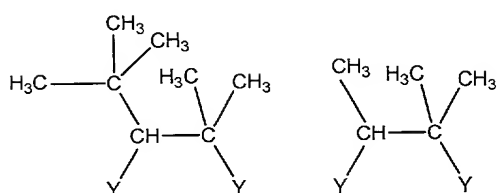
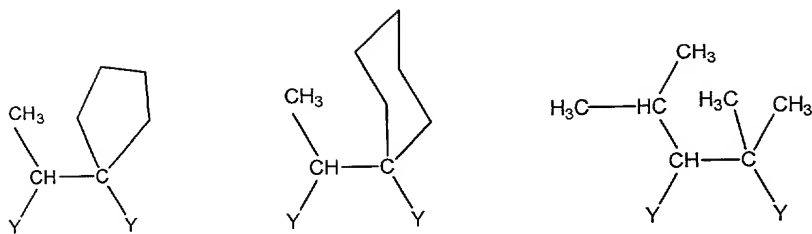
[0023] When $a = 1$, that is when there is only one Y atom, preferred T groups that can be used for those compositions represented by Group A formula include:



[0024] The following are preferred T groups when a=2 for compositions represented by Group A formulae:

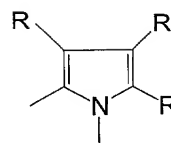
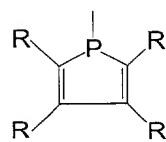
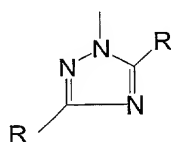
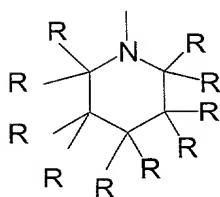
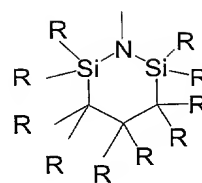
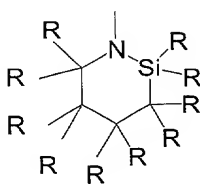
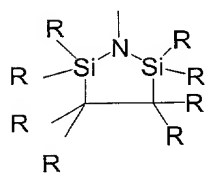
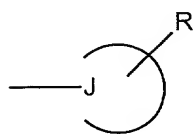


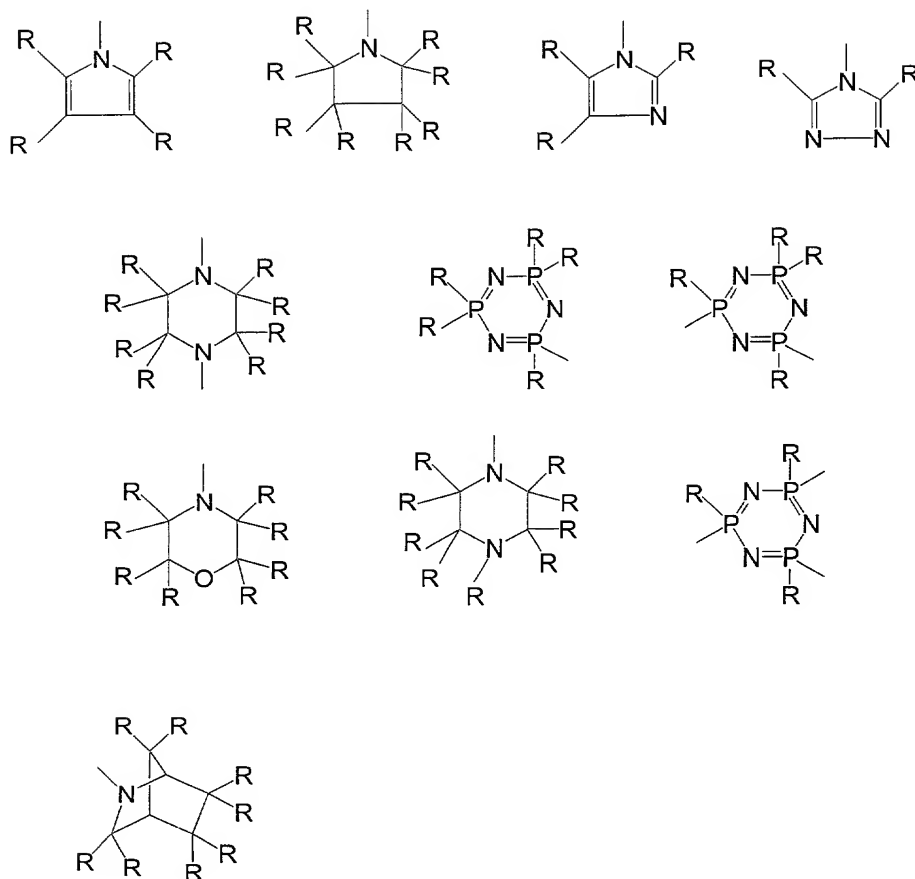
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The Y substituents are included for convenience.

[0025] Non-limiting examples of the ring structure include:





[0026] The catalyst precursors can be prepared by any suitable synthesis method and the method of synthesis is not critical to the present invention. One useful method of preparing the catalyst precursors of the present invention is by reacting a suitable metal compound, preferably one having a displaceable anionic ligand, with a heteroatom-containing ligand of this invention. Non-limiting examples of suitable metal compounds include organometallics, metal halides, sulfonates, carboxylates, phosphates, organoborates (including fluoro-containing and other subclasses), acetonacetates, sulfides, sulfates, tetrafluoroborates, nitrates, perchlorates, phenoxides, alkoxides, silicates, arsenates, borohydrides, naphthenates, cyclooctadienes, diene conjugated complexes, thiocyanates, cyanates, and the metal

cyanides. Preferred are the organometallics and the metal halides. More preferred are the organometallics.

[0027] As previously mentioned, the metal of the organometal compound may be selected from Groups 1 to 16, preferably it is a transition metal selected from Groups 3 to 13 elements and Lanthanide series elements. It is also preferred that the metal be selected from Groups 3 to 7 elements. The groups referred to are from the Periodic Table of the Elements. It is particularly preferred that the metal be a Group 4 metal, more particularly preferred is zirconium and hafnium, and most particularly preferred is zirconium.

[0028] The transition metal compound can, for example, be a metal hydrocarbyl such as: a metal alkyl, a metal aryl, a metal arylalkyl; a metal silylalkyl; a metal diene, a metal amide; or a metal phosphide. Preferably, the transition metal compound is a zirconium or hafnium hydrocarbyl. More preferably, the transition metal compound is a zirconium arylalkyl. Most preferably, the transition metal compound is tetrabenzylzirconium.

[0029] Examples of useful and preferred transition metal compounds include:

(i) tetramethylzirconium, tetraethylzirconium, zirconiumdichloride (η^4 -1,4-diphenyl-1,3-butadiene), bis (triethylphosphine) and zirconiumdichloride (η^4 -1,4-diphenyl-1,3-butadiene) bis (tri-n-propylphosphine).

tetrakis[trimethylsilylmethyl]zirconium, tetrakis [dimethylamino]zirconium, dichlorodibenzylzirconium, chlorotribenzylzirconium, trichlorobenzylzirconium, bis[dimethylamino]bis[benzyl]zirconium, and tetrabenzylzirconium;

(ii) tetramethyltitanium, tetraethyltitanium, titaniumdichloride (η^4 -1,4-diphenyl-1,3-butadiene), bis (triethylphosphine) and titaniumdichloride (η^4 -1,4-diphenyl-1,3-butadiene) bis (tri-n-propylphosphine), tetrakis[trimethylsilylmethyl]-titanium, tetrakis[dimethylamino]titanium, dichlorodibenzyltitanium,

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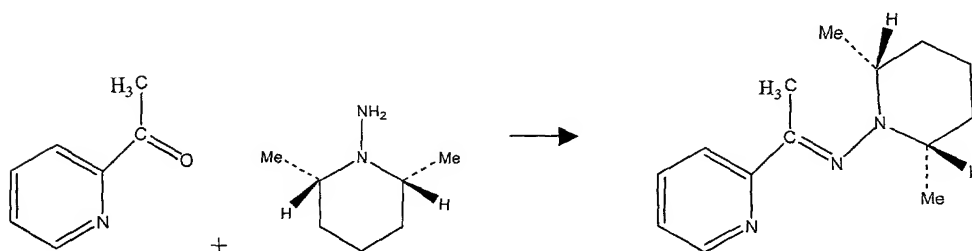
chlorotribenzyltitanium, trichlorobenzyltitanium,

bis[dimethylamino]bis[benzyl]titanium, and tetrabenzyltitanium; and

(iii) tetramethylhafnium, tetraethylhafnium, hafniumdichloride (η^4 -1,4-diphenyl-1,3-butadiene), bis (triethylphosphine) and hafniumdichloride (η^4 -1,4-diphenyl-1,3-butadiene) bis (tri-n-propylphosphine), tetrakis[trimethylsilylmethyl]hafnium, tetrakis[dimethylamino]hafnium, dichlorodibenzylhafnium, chlorotribenzylhafnium, trichlorobenzylhafnium, bis[dimethylamino]bis[benzyl]hafnium, and tetrabenzylhafnium..

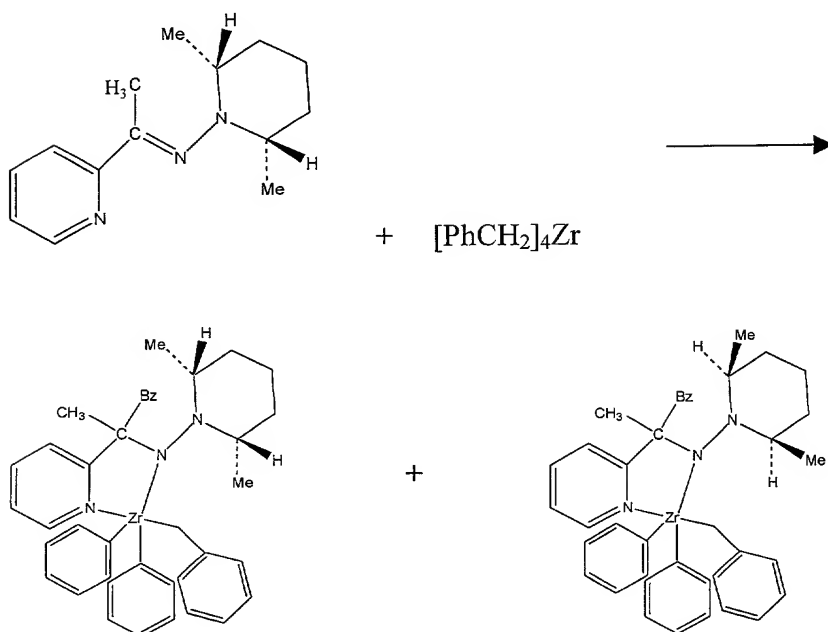
[0030] One preferred heteroatom-containing ligand that can be used in the practice of the present invention is:

The imine of 2-acetylpyridine is first synthesized.



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Reaction of the 2-acetylpyridine imine with tetrabenzyl zirconium will lead to the products shown below.



Activators and Activation Methods for Catalyst Compounds

[0031] The polymerization catalyst compounds of the invention are typically activated in various ways to yield compounds having a vacant coordination site that will coordinate, insert, and polymerize olefin(s). For the purposes of this patent specification and appended claims, the term “activator” is defined to be any compound which can activate any one of the catalyst compounds described above by converting the neutral catalyst compound to a catalytically active catalyst compound cation. Non-limiting activators, for example, include alumoxanes, aluminum alkyls, ionizing activators, which may be neutral or ionic, and conventional-type cocatalysts.

A. Alumoxane and Aluminum Alkyl Activators

[0032] In one embodiment, alumoxanes activators are utilized as an activator in the catalyst composition of the invention. Alumoxanes are generally oligomeric compounds containing -Al(R)-O- subunits, where R is an alkyl group. Examples of alumoxanes include methylalumoxane (MAO), modified methylalumoxane (MMAO), ethylalumoxane and isobutylalumoxane. Alumoxanes may be produced by the hydrolysis of the respective trialkylaluminum compound. MMAO may be produced by the hydrolysis of trimethylaluminum and a higher trialkylaluminum such as triisobutylaluminum. MMAO's are generally more soluble in aliphatic solvents and more stable during storage. There are a variety of methods for preparing alumoxane and modified alumoxanes, non-limiting examples of which are described in U.S. Patent No. 4,665,208, 4,952,540, 5,091,352, 5,206,199, 5,204,419, 4,874,734, 4,924,018, 4,908,463, 4,968,827, 5,308,815, 5,329,032, 5,248,801, 5,235,081, 5,157,137, 5,103,031, 5,391,793, 5,391,529, 5,693,838, 5,731,253, 5,731,451, 5,744,656, 5,847,177, 5,854,166, 5,856,256 and 5,939,346 and European publications EP-A-0 561 476, EP-B1-0 279 586, EP-A-0 594-218 and EP-B1-0 586 665, and PCT publications WO 94/10180 and WO 99/15534, all of which are herein fully incorporated by reference. A another alumoxane is a modified methyl alumoxane (MMAO) cocatalyst type 3A (commercially available from Akzo Chemicals, Inc. under the trade name Modified Methylalumoxane type 3A, covered under patent number US 5,041,584).

[0033] Aluminum Alkyl or organoaluminum compounds which may be utilized as activators include trimethylaluminum, triethylaluminum, triisobutylaluminum, tri-n-hexylaluminum, tri-n-octylaluminum and the like.

B. Ionizing Activators

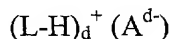
[0034] It is within the scope of this invention to use an ionizing or stoichiometric activator, neutral or ionic, such as tri (n-butyl) ammonium tetrakis (pentafluorophenyl) boron, a trisperfluorophenyl boron metalloid precursor or a

tris(perfluoronaphthyl) boron metalloid precursor, polyhalogenated heteroborane anions (WO 98/43983), boric acid (U.S. Patent No. 5,942,459) or combination thereof. It is also within the scope of this invention to use neutral or ionic activators alone or in combination with alumoxane or modified alumoxane activators.

[0035] Examples of neutral stoichiometric activators include tri-substituted boron, thallium, aluminum, gallium and indium or mixtures thereof. The three substituent groups are each independently selected from alkyls, alkenyls, halogen, substituted alkyls, aryls, arylhalides, alkoxy and halides. Preferably, the three groups are independently selected from halogen, mono or multicyclic (including halosubstituted) aryls, alkyls, and alkenyl compounds and mixtures thereof, preferred are alkenyl groups having 1 to 20 carbon atoms, alkyl groups having 1 to 20 carbon atoms, alkoxy groups having 1 to 20 carbon atoms and aryl groups having 3 to 20 carbon atoms (including substituted aryls). More preferably, the three groups are alkyls having 1 to 4 carbon groups, phenyl, naphthyl or mixtures thereof. Even more preferably, the three groups are halogenated, preferably fluorinated, aryl groups. Most preferably, the neutral stoichiometric activator is tris(perfluorophenyl) boron or tris(perfluoronaphthyl) boron.

[0036] Ionic stoichiometric activator compounds may contain an active proton, or some other cation associated with, but not coordinated to, or only loosely coordinated to, the remaining ion of the ionizing compound. Such compounds and the like are described in European publications EP-A-0 570 982, EP-A-0 520 732, EP-A-0 495 375, EP-B1-0 500 944, EP-A-0 277 003 and EP-A-0 277 004, and U.S. Patent Nos. 5,153,157, 5,198,401, 5,066,741, 5,206,197, 5,241,025, 5,384,299 and 5,502,124 and U.S. Patent Application Serial No. 08/285,380, filed August 3, 1994, all of which are herein fully incorporated by reference.

[0037] In a preferred embodiment, the stoichiometric activators include a cation and an anion component, and may be represented by the following formula:



wherein L is a neutral Lewis base;

H is hydrogen;

$(L-H)^+$ is a Bronsted acid;

A^{d-} is a non-coordinating anion having the charge d-;

d is an integer from 1 to 3.

[0038] The cation component, $(L-H)_d^+$ may include Bronsted acids such as protons or protonated Lewis bases or reducible Lewis acids capable of protonating or abstracting a moiety, such as an alkyl or aryl, from the bulky ligand metallocene or Group 15 containing transition metal catalyst precursor, resulting in a cationic transition metal species.

[0039] The activating cation $(L-H)_d^+$ may be a Bronsted acid, capable of donating a proton to the transition metal catalytic precursor resulting in a transition metal cation, including ammoniums, oxoniums, phosphoniums, silyliums and mixtures thereof, preferably ammoniums of methylamine, aniline, dimethylamine, diethylamine, N-methylaniline, diphenylamine, trimethylamine, triethylamine, N,N-dimethylaniline, methyldiphenylamine, pyridine, p-bromo N,N-dimethylaniline, p-nitro-N,N-dimethylaniline, phosphoniums from triethylphosphine, triphenylphosphine, and diphenylphosphine, oxoniums from ethers such as dimethyl ether diethyl ether, tetrahydrofuran and dioxane, sulfoniums from thioethers, such as diethyl thioethers and tetrahydrothiophene and mixtures thereof. The activating cation $(L-H)_d^+$ may also be an abstracting moiety such as silver, carboniums, tropylium, carbeniums, ferroceniums and mixtures, preferably carboniums and ferroceniums. Most preferably $(L-H)_d^+$ is triphenyl carbonium.

[0040] The anion component A^{d-} include those having the formula $[M^{k+}Q_n]^{d-}$ wherein k is an integer from 1 to 3; n is an integer from 2-6; $n - k = d$; M is an element selected from Group 13 of the Periodic Table of the Elements, preferably boron or aluminum, and Q is independently a hydride, bridged or unbridged dialkylamido, halide, alkoxide, aryloxy, hydrocarbyl, substituted hydrocarbyl, halocarbyl, substituted halocarbyl, and halosubstituted-hydrocarbyl radicals, said Q having up to 20 carbon atoms with the proviso that in not more than 1 occurrence is Q a halide. Preferably, each Q is a fluorinated hydrocarbyl group having 1 to 20 carbon atoms, more preferably each Q is a fluorinated aryl group, and most preferably each Q is a pentafluoryl aryl group. Examples of suitable A^{d-} also include diboron compounds as disclosed in U.S. Pat. No. 5,447,895, which is fully incorporated herein by reference.

[0041] Most preferably, the ionic stoichiometric activator $(L-H)_d^+ (A^{d-})$ is N,N-dimethylanilinium tetra(perfluorophenyl)borate or triphenylcarbenium tetra(perfluorophenyl)borate.

[0042] In one embodiment, an activation method using ionizing ionic compounds not containing an active proton but capable of producing a bulky ligand metallocene catalyst cation and their non-coordinating anion are also contemplated, and are described in EP-A- 0 426 637, EP-A- 0 573 403 and U.S. Patent No. 5,387,568, which are all herein incorporated by reference.

Supports, Carriers and General Supporting Techniques

[0043] Although not preferred, the catalyst system of the invention can include a support material or carrier, or a supported activator. For example, the catalyst compound of the invention can be deposited on, contacted with, vaporized with, bonded to, or incorporated within, adsorbed or absorbed in, or on, a support or carrier.

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A. Support Material

[0044] The support material, if used, can be any of the conventional support materials. Preferably the supported material is a porous support material, for example, talc, inorganic oxides and inorganic chlorides. Other support materials include resinous support materials such as polystyrene, functionalized or crosslinked organic supports, such as polystyrene divinyl benzene polyolefins or polymeric compounds, zeolites, clays, or any other organic or inorganic support material and the like, or mixtures thereof.

[0045] The preferred support materials are inorganic oxides that include those Group 2, 3, 4, 5, 13 or 14 metal oxides. The preferred supports include silica, fumed silica, alumina (WO 99/60033), silica-alumina and mixtures thereof. Other useful supports include magnesia, titania, zirconia, magnesium chloride (U.S. Patent No. 5,965,477), montmorillonite (European Patent EP-B1 0 511 665), phyllosilicate, zeolites, talc, clays (U.S. Patent No. 6,034,187) and the like. Also, combinations of these support materials may be used, for example, silica-chromium, silica-alumina, silica-titania and the like. Additional support materials may include those porous acrylic polymers described in EP 0 767 184 B1, which is incorporated herein by reference. Other support materials include nanocomposites as described in PCT WO 99/47598, aerogels as described in WO 99/48605, spherulites as described in U.S. Patent No. 5,972,510 and polymeric beads as described in WO 99/50311, which are all herein incorporated by reference. A preferred support is fumed silica available under the trade name Cabosil™ TS-610, available from Cabot Corporation. Fumed silica is typically a silica with particles 7 to 30 nanometers in size that has been treated with dimethylsilyldichloride such that a majority of the surface hydroxyl groups are capped.

[0046] It is preferred that the support material, most preferably an inorganic oxide, has a surface area in the range of from about 10 to about 700 m²/g, pore volume in

the range of from about 0.1 to about 4.0 cc/g and average particle size in the range of from about 5 to about 500 μm . More preferably, the surface area of the support material is in the range of from about 50 to about 500 m^2/g , pore volume of from about 0.5 to about 3.5 cc/g and average particle size of from about 10 to about 200 μm . Most preferably the surface area of the support material is in the range is from about 100 to about 400 m^2/g , pore volume from about 0.8 to about 3.0 cc/g and average particle size is from about 5 to about 100 μm . The average pore size of the carrier of the invention typically has pore size in the range of from 10 to 1000Å, preferably 50 to about 500Å, and most preferably 75 to about 350Å.

[0047] The support materials may be treated chemically, for example with a fluoride compound as described in WO 00/12565, which is herein incorporated by reference. Other supported activators are described in for example WO 00/13792 that refers to supported boron containing solid acid complex.

[0048] In a preferred method of forming a supported catalyst composition component, the amount of liquid in which the activator is present is in an amount that is less than four times the pore volume of the support material, more preferably less than three times, even more preferably less than two times; preferred ranges being from 1.1 times to 3.5 times range and most preferably in the 1.2 to 3 times range. In an alternative embodiment, the amount of liquid in which the activator is present is from one to less than one times the pore volume of the support material utilized in forming the supported activator.

[0049] Procedures for measuring the total pore volume of a porous support are well known in the art. Details of one of these procedures is discussed in Volume 1, *Experimental Methods in Catalytic Research* (Academic Press, 1968) (specifically see pages 67-96). This preferred procedure involves the use of a classical BET apparatus for nitrogen absorption. Another method well known in the art is described in Innes,

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Total Porosity and Particle Density of Fluid Catalysts By Liquid Titration, Vol. 28, No. 3, Analytical Chemistry 332-334 (March, 1956).

B. Supported Activators

[0050] In one embodiment, the catalyst composition includes a supported activator. Many supported activators are described in various patents and publications which include: U.S. Patent No. 5,728,855 directed to the forming a supported oligomeric alkylaluminumoxane formed by treating a trialkylaluminum with carbon dioxide prior to hydrolysis; U.S. Patent No. 5,831,109 and 5,777,143 discusses a supported methylalumoxane made using a non-hydrolytic process; U.S. Patent No. 5,731,451 relates to a process for making a supported alumoxane by oxygenation with a trialkylsiloxo moiety; U.S. Patent No. 5,856,255 discusses forming a supported auxiliary catalyst (alumoxane or organoboron compound) at elevated temperatures and pressures; U.S. Patent No. 5,739,368 discusses a process of heat treating alumoxane and placing it on a support; EP-A-0 545 152 relates to adding a metallocene to a supported alumoxane and adding more methylalumoxane; U.S. Patent Nos. 5,756,416 and 6,028,151 discuss a catalyst composition of a alumoxane impregnated support and a metallocene and a bulky aluminum alkyl and methylalumoxane; EP-B1-0 662 979 discusses the use of a metallocene with a catalyst support of silica reacted with alumoxane; PCT WO 96/16092 relates to a heated support treated with alumoxane and washing to remove unfixed alumoxane; U.S. Patent Nos. 4,912,075, 4,937,301, 5,008,228, 5,086,025, 5,147,949, 4,871,705, 5,229,478, 4,935,397, 4,937,217 and 5,057,475, and PCT WO 94/26793 all directed to adding a metallocene to a supported activator; U.S. Patent No. 5,902,766 relates to a supported activator having a specified distribution of alumoxane on the silica particles; U.S. Patent No. 5,468,702 relates to aging a supported activator and adding a metallocene; U.S. Patent No. 5,968,864 discusses treating a solid with alumoxane and introducing a metallocene; EP 0 747 430 A1 relates to a process using a metallocene on a supported methylalumoxane and trimethylaluminum; EP 0 969 019 A1 discusses the use of a metallocene and a supported activator; EP-B2-0 170 059

relates to a polymerization process using a metallocene and a organo-aluminum compound, which is formed by reacting aluminum trialkyl with a water containing support; U.S. Patent No. 5,212,232 discusses the use of a supported alumoxane and a metallocene for producing styrene based polymers; U.S. Patent No. 5,026,797 discusses a polymerization process using a solid component of a zirconium compound and a water-insoluble porous inorganic oxide preliminarily treated with alumoxane; U.S. Patent No. 5,910,463 relates to a process for preparing a catalyst support by combining a dehydrated support material, an alumoxane and a polyfunctional organic crosslinker; U.S. Patent Nos. 5,332,706, 5,473,028, 5,602,067 and 5,420,220 discusses a process for making a supported activator where the volume of alumoxane solution is less than the pore volume of the support material; WO 98/02246 discusses silica treated with a solution containing a source of aluminum and a metallocene; WO 99/03580 relates to the use of a supported alumoxane and a metallocene; EP-A1-0 953 581 discloses a heterogeneous catalytic system of a supported alumoxane and a metallocene; U.S. Patent No. 5,015,749 discusses a process for preparing a polyhydrocarbyl-alumoxane using a porous organic or inorganic imbibitor material; U.S. Patent Nos. 5,446,001 and 5,534,474 relates to a process for preparing one or more alkylaluminumoxanes immobilized on a solid, particulate inert support; and EP-A1-0 819 706 relates to a process for preparing a solid silica treated with alumoxane. Also, the following articles, also fully incorporated herein by reference for purposes of disclosing useful supported activators and methods for their preparation, include: W. Kaminsky, et al., "Polymerization of Styrene with Supported Half-Sandwich Complexes", Journal of Polymer Science Vol. 37, 2959-2968 (1999) describes a process of adsorbing a methylalumoxane to a support followed by the adsorption of a metallocene; Juntong Xu, et al. "Characterization of isotactic polypropylene prepared with dimethylsilyl bis(1-indenyl)zirconium dichloride supported on methylaluminoxane pretreated silica", European Polymer Journal 35 (1999) 1289-1294, discusses the use of silica treated with methylalumoxane and a metallocene; Stephen O'Brien, et al., "EXAFS analysis of a chiral alkene polymerization catalyst incorporated in the mesoporous silicate MCM-41" Chem. Commun. 1905-1906

(1997) discloses an immobilized alumoxane on a modified mesoporous silica; and F.Bonini, et al., "Propylene Polymerization through Supported Metallocene/MAO Catalysts: Kinetic Analysis and Modeling" Journal of Polymer Science, Vol. 33 2393-2402 (1995) discusses using a methylalumoxane supported silica with a metallocene. Any of the methods discussed in these references are useful for producing the supported activator component utilized in the catalyst composition of the invention and all are incorporated herein by reference.

[0051] In another embodiment, the supported activator, such as supported alumoxane, is aged for a period of time prior to use herein. For reference please refer to U.S. Patent Nos. 5,468,702 and 5,602,217, incorporated herein by reference.

[0052] In an embodiment, the supported activator is in a dried state or a solid. In another embodiment, the supported activator is in a substantially dry state or a slurry, preferably in a mineral oil slurry.

[0053] In another embodiment, two or more separately supported activators are used, or alternatively, two or more different activators on a single support are used.

[0054] In another embodiment, the support material, preferably partially or totally dehydrated support material, preferably 200°C to 600°C dehydrated silica, is then contacted with an organoaluminum or alumoxane compound. Preferably in an embodiment where an organoaluminum compound is used, the activator is formed in situ on and in the support material as a result of the reaction of, for example, trimethylaluminum and water.

[0055] In another embodiment, Lewis base-containing supports are reacted with a Lewis acidic activator to form a support bonded Lewis acid compound. The Lewis base hydroxyl groups of silica are exemplary of metal/metalloid oxides where this

method of bonding to a support occurs. This embodiment is described in U.S. Patent Application No. 09/191,922, filed November 13, 1998, which is herein incorporated by reference.

[0056] Other embodiments of supporting an activator are described in U.S. Patent No. 5,427,991, where supported non-coordinating anions derived from tris(perfluorophenyl) boron are described; U.S. Patent No. 5,643,847 discusses the reaction of Group 13 Lewis acid compounds with metal oxides such as silica and illustrates the reaction of tris(perfluorophenyl) boron with silanol groups (the hydroxyl groups of silicon) resulting in bound anions capable of protonating transition metal organometallic catalyst compounds to form catalytically active cations counter-balanced by the bound anions; immobilized Group IIIA Lewis acid catalysts suitable for carbocationic polymerizations are described in U.S. Patent No. 5,288,677; and James C.W. Chien, Jour. Poly. Sci.: Pt A: Poly. Chem, Vol. 29, 1603 - 1607 (1991), describes the olefin polymerization utility of methylalumoxane (MAO) reacted with silica (SiO_2) and metallocenes and describes a covalent bonding of the aluminum atom to the silica through an oxygen atom in the surface hydroxyl groups of the silica.

[0057] In a preferred embodiment, a supported activator is formed by preparing in an agitated, and temperature and pressure controlled vessel a solution of the activator and a suitable solvent, then adding the support material at temperatures from 0°C to 100°C , contacting the support with the activator solution for up to 24 hours, then using a combination of heat and pressure to remove the solvent to produce a free flowing powder. Temperatures can range from 40 to 120°C and pressures from 5 psia to 20 psia (34.5 to 138kPa). An inert gas sweep can also be used in assist in removing solvent. Alternate orders of addition, such as slurrying the support material in an appropriate solvent then adding the activator, can be used.

Polymerization Process

[0058] The catalyst systems prepared and the method of catalyst system addition described above are suitable for use in any prepolymerization and/or polymerization process over a wide range of temperatures and pressures. The temperatures may be in the range of from -60 °C to about 280°C, preferably from 50°C to about 200°C, and the pressures employed may be in the range from 1 atmosphere to about 500 atmospheres or higher.

[0059] Polymerization processes include solution, gas phase, slurry phase and a high pressure process or a combination thereof. Particularly preferred is a gas phase or slurry phase polymerization of one or more olefins at least one of which is ethylene or propylene.

[0060] In one embodiment, the process of this invention is directed toward a solution, high pressure, slurry or gas phase polymerization process of one or more olefin monomers having from 2 to 30 carbon atoms, preferably 2 to 12 carbon atoms, and more preferably 2 to 8 carbon atoms. The invention is particularly well suited to the polymerization of two or more olefin monomers of ethylene, propylene, butene-1, pentene-1, 4-methyl-pentene-1, hexene-1, octene-1 and decene-1.

[0061] Other monomers useful in the process of the invention include ethylenically unsaturated monomers, diolefins having 4 to 18 carbon atoms, conjugated or nonconjugated dienes, polyenes, vinyl monomers and cyclic olefins. Non-limiting monomers useful in the invention may include norbornene, norbornadiene, isobutylene, isoprene, vinylbenzocyclobutane, styrenes, alkyl substituted styrene, ethylidene norbornene, dicyclopentadiene and cyclopentene.

[0062] In the most preferred embodiment of the process of the invention, a copolymer of ethylene is produced, where with ethylene, a comonomer having at least one alpha-olefin having from 3 to 15 carbon atoms, preferably from 4 to 12 carbon atoms, and most preferably from 4 to 8 carbon atoms, is polymerized in a gas phase process.

[0063] In another embodiment of the process of the invention, ethylene or propylene is polymerized with at least two different comonomers, optionally one of which may be a diene, to form a terpolymer.

[0064] In an embodiment, the mole ratio of comonomer to ethylene, C_x/C_2 , where C_x is the amount of comonomer and C_2 is the amount of ethylene is between about 0.001 to 0.200 and more preferably between about 0.002 to 0.008.

[0065] In one embodiment, the invention is directed to a polymerization process, particularly a gas phase or slurry phase process, for polymerizing propylene alone or with one or more other monomers including ethylene, and/or other olefins having from 4 to 12 carbon atoms. Polypropylene polymers may be produced using the particularly bridged bulky ligand metallocene catalysts as described in U.S. Patent Nos. 5,296,434 and 5,278,264, both of which are herein incorporated by reference.

[0066] Typically in a gas phase polymerization process a continuous cycle is employed where in one part of the cycle of a reactor system, a cycling gas stream, otherwise known as a recycle stream or fluidizing medium, is heated in the reactor by the heat of polymerization. This heat is removed from the recycle composition in another part of the cycle by a cooling system external to the reactor. Generally, in a gas fluidized bed process for producing polymers, a gaseous stream containing one or more monomers is continuously cycled through a fluidized bed in the presence of a catalyst under reactive conditions. The gaseous stream is withdrawn from the fluidized bed and recycled back into the reactor. Simultaneously, polymer product is

withdrawn from the reactor and fresh monomer is added to replace the polymerized monomer. (See for example U.S. Patent Nos. 4,543,399, 4,588,790, 5,028,670, 5,317,036, 5,352,749, 5,405,922, 5,436,304, 5,453,471, 5,462,999, 5,616,661 and 5,668,228, all of which are fully incorporated herein by reference.)

[0067] The reactor pressure in a gas phase process may vary from about 100 psig (690 kPa) to about 600 psig (4138 kPa), preferably in the range of from about 200 psig (1379 kPa) to about 400 psig (2759 kPa), more preferably in the range of from about 250 psig (1724 kPa) to about 350 psig (2414 kPa).

[0068] The reactor temperature in a gas phase process may vary from about 30°C to about 120°C, preferably from about 60°C to about 115°C, more preferably in the range of from about 70°C to 110°C, and most preferably in the range of from about 70°C to about 95°C.

[0069] Other gas phase processes contemplated by the process of the invention include series or multistage polymerization processes. Also gas phase processes contemplated by the invention include those described in U.S. Patent Nos. 5,627,242, 5,665,818 and 5,677,375, and European publications EP-A- 0 794 200 EP-B1-0 649 992, EP-A- 0 802 202 and EP-B- 634 421 all of which are herein fully incorporated by reference.

[0070] In a preferred embodiment, the reactor utilized in the present invention is capable of and the process of the invention is producing greater than 500 lbs of polymer per hour (227 Kg/hr) to about 200,000 lbs/hr (90,900 Kg/hr) or higher of polymer, preferably greater than 1000 lbs/hr (455 Kg/hr), more preferably greater than 10,000 lbs/hr (4540 Kg/hr), even more preferably greater than 25,000 lbs/hr (11,300 Kg/hr), still more preferably greater than 35,000 lbs/hr (15,900 Kg/hr), still even more preferably greater than 50,000 lbs/hr (22,700 Kg/hr) and most preferably

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greater than 65,000 lbs/hr (29,000 Kg/hr) to greater than 100,000 lbs/hr (45,500 Kg/hr).

[0071] A slurry polymerization process generally uses pressures in the range of from about 1 to about 50 atmospheres and even greater and temperatures in the range of 0°C to about 120°C. In a slurry polymerization, a suspension of solid, particulate polymer is formed in a liquid polymerization diluent medium to which ethylene and comonomers and often hydrogen along with catalyst are added. The suspension including diluent is intermittently or continuously removed from the reactor where the volatile components are separated from the polymer and recycled, optionally after a distillation, to the reactor. The liquid diluent employed in the polymerization medium is typically an alkane having from 3 to 7 carbon atoms, preferably a branched alkane. The medium employed should be liquid under the conditions of polymerization and relatively inert. When a propane medium is used the process must be operated above the reaction diluent critical temperature and pressure. Preferably, a hexane or an isobutane medium is employed.

[0072] A preferred polymerization technique of the invention is referred to as a particle form polymerization, or a slurry process where the temperature is kept below the temperature at which the polymer goes into solution. Such technique is well known in the art, and described in for instance U.S. Patent No. 3,248,179 which is fully incorporated herein by reference. Other slurry processes include those employing a loop reactor and those utilizing a plurality of stirred reactors in series, parallel, or combinations thereof. Non-limiting examples of slurry processes include continuous loop or stirred tank processes. Also, other examples of slurry processes are described in U.S. Patent No. 4,613,484 and 5,986,021, which are herein fully incorporated by reference.

[0073] In an embodiment the reactor used in the slurry process of the invention is capable of and the process of the invention is producing greater than 2000 lbs of polymer per hour (907 Kg/hr), more preferably greater than 5000 lbs/hr (2268 Kg/hr), and most preferably greater than 10,000 lbs/hr (4540 Kg/hr). In another embodiment the slurry reactor used in the process of the invention is producing greater than 15,000 lbs of polymer per hour (6804 Kg/hr), preferably greater than 25,000 lbs/hr (11,340 Kg/hr) to about 100,000 lbs/hr (45,500 Kg/hr). Examples of solution processes are described in U.S. Patent Nos. 4,271,060, 5,001,205, 5,236,998, 5,589,555 and 5,977,251 and PCT WO 99/32525 and PCT WO 99/40130, which are fully incorporated herein by reference

[0074] A preferred process of the invention is where the process, preferably a slurry or gas phase process is operated in the presence of a bulky ligand metallocene catalyst system of the invention and in the absence of or essentially free of any scavengers, such as triethylaluminum, trimethylaluminum, tri-isobutylaluminum and tri-n-hexylaluminum and diethyl aluminum chloride, dibutyl zinc and the like. This preferred process is described in PCT publication WO 96/08520 and U.S. Patent No. 5,712,352 and 5,763,543, which are herein fully incorporated by reference.

[0075] In one embodiment of the invention, olefin(s), preferably C₂ to C₃₀ olefin(s) or alpha-olefin(s), preferably ethylene or propylene or combinations thereof are prepolymerized in the presence of the metallocene catalyst systems of the invention described above prior to the main polymerization. The prepolymerization can be carried out batchwise or continuously in gas, solution or slurry phase including at elevated pressures. The prepolymerization can take place with any olefin monomer or combination and/or in the presence of any molecular weight controlling agent such as hydrogen. For examples of prepolymerization procedures, see U.S. Patent Nos. 4,748,221, 4,789,359, 4,923,833, 4,921,825, 5,283,278 and 5,705,578 and European

publication EP-B-0279 863 and PCT Publication WO 97/44371 all of which are herein fully incorporated by reference.

[0076] In one embodiment, toluene is not used in the preparation or polymerization process of this invention.

Polymer Products

[0077] The polymers produced by the process of the invention can be used in a wide variety of products and end-use applications. The polymers produced by the process of the invention include linear low density polyethylene, elastomers, plastomers, high density polyethylenes, medium density polyethylenes, low density polyethylenes, polypropylene and polypropylene copolymers. Also produced are isotactic polymers, such as poly-1-hexene and bimodal polyethylene.

[0078] The polymers, typically ethylene based polymers, have a density in the range of from 0.86g/cc to 0.97 g/cc, preferably in the range of from 0.88 g/cc to 0.965 g/cc, more preferably in the range of from 0.900 g/cc to 0.96 g/cc, even more preferably in the range of from 0.905 g/cc to 0.95 g/cc, yet even more preferably in the range from 0.910 g/cc to 0.940 g/cc, and most preferably greater than 0.915 g/cc, preferably greater than 0.920 g/cc, and most preferably greater than 0.925 g/cc. Density is measured in accordance with ASTM-D-1238.

[0079] The polymers produced by the process of the invention typically have a molecular weight distribution, a weight average molecular weight to number average molecular weight (M_w/M_n) of greater than 1.5 to about 30, particularly greater than 2 to about 10, more preferably greater than about 2.2 to less than about 8, and most preferably from 2.5 to 8.

[0080] Also, the polymers of the invention typically have a narrow composition distribution as measured by Composition Distribution Breadth Index (CDBI). Further

details of determining the CDBI of a copolymer are known to those skilled in the art. See, for example, PCT Patent Application WO 93/03093, published February 18, 1993, which is fully incorporated herein by reference.

[0081] The polymers of the invention in one embodiment have CDBI's generally in the range of greater than 50% to 100%, preferably 99%, preferably in the range of 55% to 85%, and more preferably 60% to 80%, even more preferably greater than 60%, still even more preferably greater than 65%.

[0082] In another embodiment, polymers produced using a catalyst system of the invention have a CDBI less than 50%, more preferably less than 40%, and most preferably less than 30%.

[0083] The polymers of the present invention in one embodiment have a melt index (MI) or (I_2) as measured by ASTM-D-1238-E in the range from no measurable flow to 1000 dg/min, more preferably from about 0.01 dg/min to about 100 dg/min, even more preferably from about 0.1 dg/min to about 50 dg/min, and most preferably from about 0.1 dg/min to about 10 dg/min.

[0084] The polymers of the invention in an embodiment have a melt index ratio (I_{21}/I_2) (I_{21} is measured by ASTM-D-1238-F) of from 10 to less than 25, more preferably from about 15 to less than 25.

[0085] The polymers of the invention in a preferred embodiment have a melt index ratio (I_{21}/I_2) (I_{21} is measured by ASTM-D-1238-F) of from preferably greater than 25, more preferably greater than 30, even more preferably greater than 40, still even more preferably greater than 50 and most preferably greater than 65. In an embodiment, the polymer of the invention may have a narrow molecular weight distribution and a broad composition distribution or vice-versa, and may be those polymers described in U.S. Patent No. 5,798,427 incorporated herein by reference.

[0086] In yet another embodiment, propylene based polymers are produced in the process of the invention. These polymers include atactic polypropylene, isotactic polypropylene, hemi-isotactic and syndiotactic polypropylene. Other propylene polymers include propylene block or impact copolymers. Propylene polymers of these types are well known in the art see for example U.S. Patent Nos. 4,794,096, 3,248,455, 4,376,851, 5,036,034 and 5,459,117, all of which are herein incorporated by reference.

[0087] The polymers of the invention may be blended and/or coextruded with any other polymer. Non-limiting examples of other polymers include linear low density polyethylenes, elastomers, plastomers, high pressure low density polyethylene, high density polyethylenes, polypropylenes and the like.

[0088] Polymers produced by the process of the invention and blends thereof are useful in such forming operations as film, sheet, and fiber extrusion and co-extrusion as well as blow molding, injection molding and rotary molding. Films include blown or cast films formed by coextrusion or by lamination useful as shrink film, cling film, stretch film, sealing films, oriented films, snack packaging, heavy duty bags, grocery sacks, baked and frozen food packaging, medical packaging, industrial liners, membranes, etc. in food-contact and non-food contact applications. Fibers include melt spinning, solution spinning and melt blown fiber operations for use in woven or non-woven form to make filters, diaper fabrics, medical garments, geotextiles, etc. Extruded articles include medical tubing, wire and cable coatings, pipe, geomembranes, and pond liners. Molded articles include single and multi-layered constructions in the form of bottles, tanks, large hollow articles, rigid food containers and toys, etc.

[0089] The present invention will be illustrated in more detail with reference to the following examples, which should not be construed to be limiting in scope of the present invention.

Glossary

[0090] Activity is measured in g of polyethylene/mmol of metal per hr at 100 psig ethylene.

[0091] I2 is the flow index (dg/min) as measured by ASTM D-1238-Condition E at 190°C.

[0092] I21 is the flow index (dg/min) as measured by ASTM D-1238-Condition F.

[0093] MFR is the Melt Flow Ratio, I21/I2.

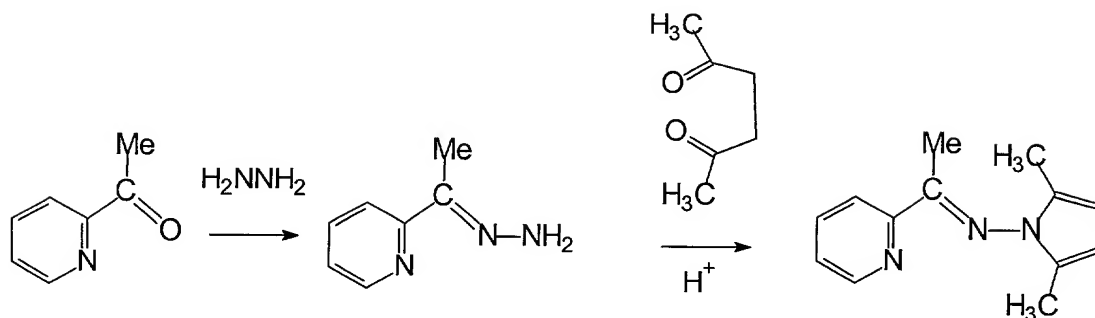
[0094] MMAO is a solution of modified methylalumoxane in heptane, approximately 1.9 molar in aluminum, commercially available from Akzo Chemicals, Inc. (type 3).

[0095] BBF is Butyl Branching Frequency, number of butyl branches per 1000 main chain carbon atoms, as determined by infrared measurement techniques.

[0096] M_w is Weight Average Molecular Weight, as determined by gel permeation chromatography using crosslinked polystyrene columns; pore size sequence: 1 column less than 1000 Å, 3 columns of mixed 5×10^7 Å; 1,2,4-trichlorobenzene solvent at 140°C, with refractive index detection. M_n is number average molecular weight.

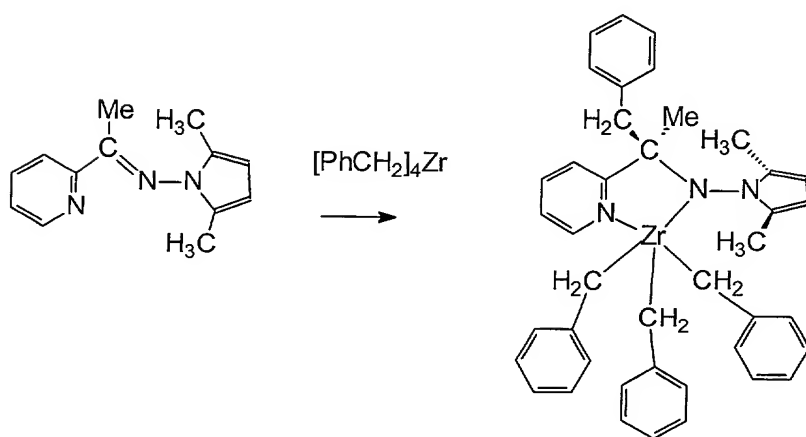
[0097] PDI is the Polydispersity Index, equivalent to Molecular Weight Distribution (M_w/M_n).

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EXAMPLES**[0098] Synthesis of 2-Acetylpyridine hydrazine adduct and 2-Acetylpyridine{N-1-2,5 dimethylpyrrole}imine**

[0099] General procedure: 2-Acetylpyridine (5.0g, 41.3 mmol) was charged to a flask equipped with a stir bar. Hydrazine (1.33g, 41.3 mmol) was added dropwise to the stirring 2-acetylpyridine. The exothermic reaction was allowed to cool to room temperature and solidify. The solids were reacted with acetonyl acetone (1 equivalent, 2 equivalents and 10 equivalents) in three separate reaction with hydrochloric acid (1 equivalent) in ether solvent. The reaction was heated to 60°C. The product was isolated.

[00100] Reaction of N-PyrroliImine Ligand with Tetrabenzyl zirconium



[00101] General procedure: In dry the box tetrabenzyl zirconium (0.200mmol, 0.091g) was charged to a 7 mL amber bottle equipped with a stir bar and cap. Benzene- d_6 (1.5 mL) was added and stirred to dissolve. To a vial was charged N-pyrroliimine ligand (0.200 mmol, 0.042 g) and 1.5 mL Benzene- d_6 . The ligand solution was transferred into the tetrabenzyl zirconium solution.

[00102] NMR analysis revealed (Composition 45% complex, 55% tetrabenzylzirconium).

[00103] This complex exhibited ethylene polymerization activity in a slurry reactor with modified methylalumoxane cocatalyst. This result clearly demonstrates proof of concept for 2,5-disubstituted amide complexes as olefin polymerization catalysts.

MMAO Cocatalyst

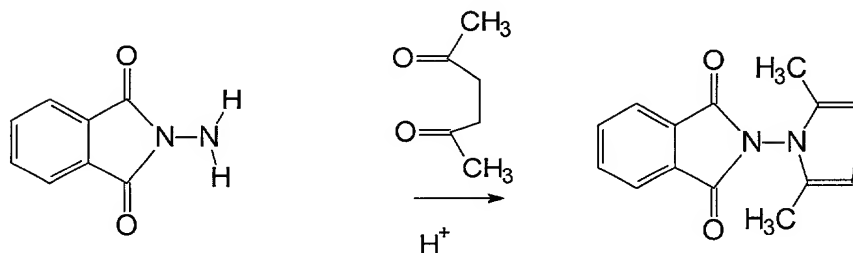
Temp,C	micromolesZr	Activity	I2	I21	MFR	BBF
85	10.0	5,106	0.232	65.39	281	14.0
85	1.0	8,471	4.16	257	61.64	15.08
65	1.0	36,235	0.268	19.62	73.23	14.3

[00104] Reaction Conditions: 85°C, 600 mL hexane, 43 mL 1-hexene, MMAO, MMAO/Zr = 1,000.

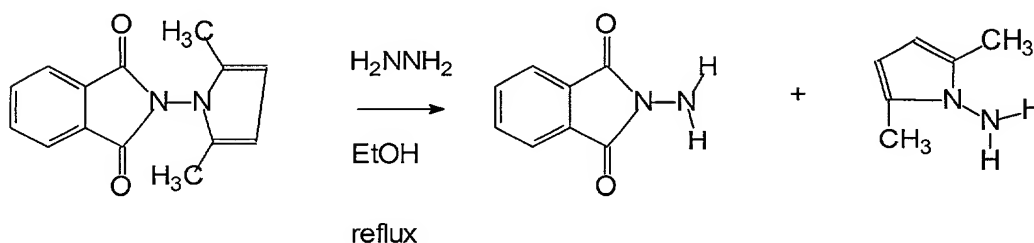
[00105] As mentioned above the ^1H -nmr analysis was 45% pyridylamidepyrrole-zirconiumtribenzyl complex plus 55% tetrabenzylzirconium. The tetrabenzylzirconium was apparently employed in excess over ligand. Hence 10.0 micromoles probably translates to 4.5 micromoles of pyridylamidepyrrolezirconiumtribenzyl complex.

[00106] In essence the true activities are likely a little more than double those shown in the table above.

[00107] Synthesis of N-amino-2,5-dimethylpyrrole



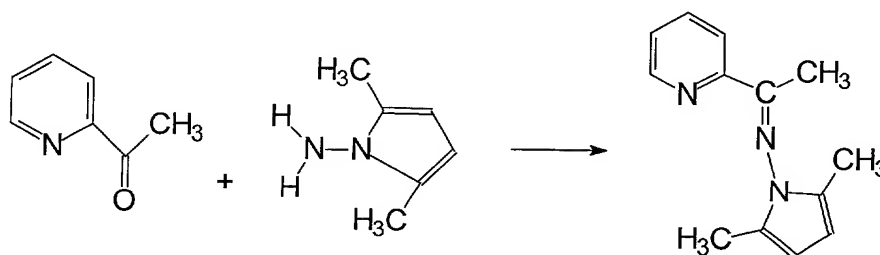
[00108] **General procedure:** N-aminophthalimide (5.35g), acetonyl acetone (3.77g) and acetic acid (60 mL) were combined in a flask equipped with a stir bar. A cold water condenser was attached and the reaction mixture was refluxed for 2 hrs. The reaction mixture was allowed to cool to room temperature and filtered. The collected solids were dried in a vacuum oven. The filtrate was mixed with water then extracted with methylene chloride. The extracts were washed with water, dried and vacuum stripped. Both samples were analyzed by ^1H NMR and appeared to be substantially the same compound.



[00109] Hydrazine (27.9 mmol, 0.89g) was added dropwise to a solution of the above product (27.9 mmol, 6.7g) in ethanol. The reaction was heated to reflux for 0.5 hours. Some of the product precipitated during the reaction. Addition of acetic acid completed the precipitation. The solids were collected by filtration. Water was added to the filtrate and neutralized with Na_2CO_3 . Excess ammonia added and the mixture was extracted with ether. The extracts were vacuum stripped to a residue.

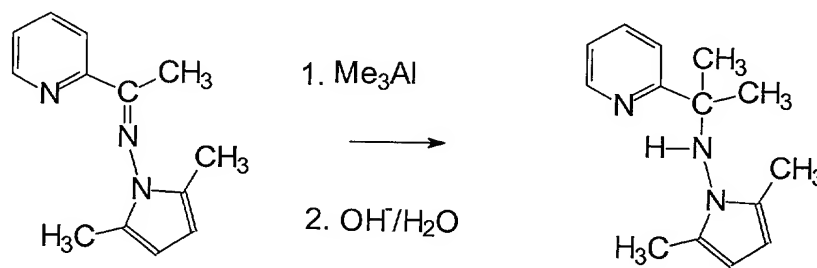
Reference: Flitsch, W., Kamer, U., Zimmermann, H.; Chem. Ber. 1969, 102, 3268-3276.

[00110] **Reaction of N-1-Amino-2,5-Dimethyl pyrrole with 2-Acetylpyridine**



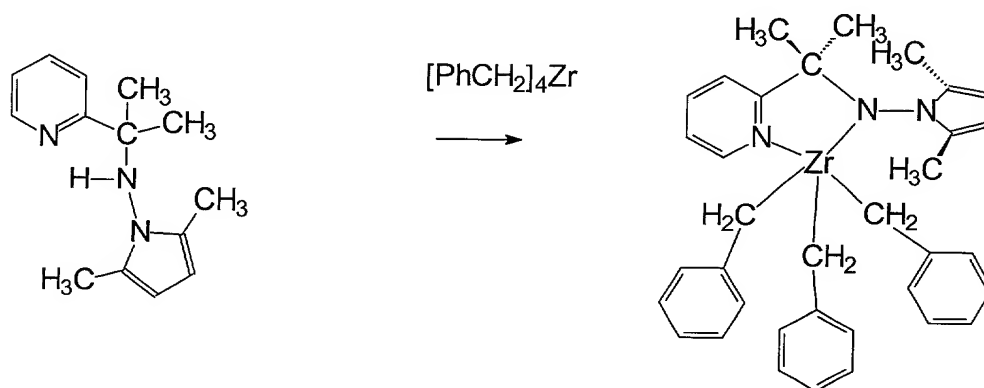
[00111] **General procedure:** The above N1-amino-2,5-dimethylpyrrole (31.1 mmol, 3.42g) was dissolved in benzene. 2-Acetylpyridine (31.1 mmol, 3.76g) and hydrochloric acid (0.11g, [1.0M solution in ether]) were added. The reaction was allowed to stir for 3 hours. The reaction was washed with water, extract with ether, washed with brine. The extracts were vacuum stripped to isolate the product.

[00112] **Alkylation of 2-Acetylpyridine, (N-1-Amino-2,5-Dimethyl pyrrole)imine**



[00113] **General procedure:** The 2-acetylpyridine, (N-1-amino-2,5-dimethyl pyrrole)imine (4.87g) was dissolved in Benzene and chilled to 0°C. Trimethyl aluminum (1 equivalent) was added dropwise. The reaction was allowed to slowly warm to room temperature. When complete the reaction was transferred in stirring KOH/H₂O, extracted with ether and vacuum stripped to a liquid residue.

[00114] **Reaction of Alkylated 2-Acetylpyridine, (N-1-Amino-2,5-Dimethyl pyrrole) imine with Tetrabenzyl zirconium**



[00115] **General procedure:** In dry the box tetrabenzyl zirconium (0.200mmol, 0.091g) was charged to a 7 mL amber bottle equipped with a stir bar and cap. Benzene-d₆ (1.5 mL) was added and stirred to dissolve. To a vial was charged the amine derived from methylation of 2-acetylpyridine, (N-1-amino-2,5-dimethyl pyrrole) imine (0.200 mmol, 0.046 g) and 1.5 mL Benzene-d₆. The ligand solution was transferred into the tetrabenzyl zirconium solution. The reaction was allowed to stir at room temperature overnight .

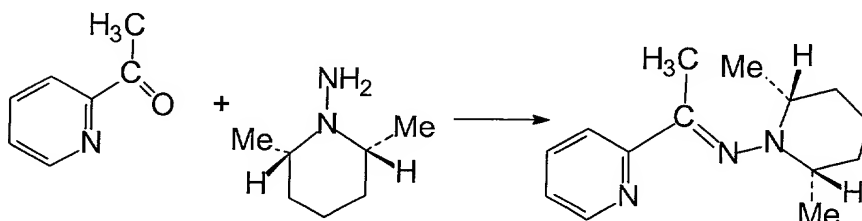
MMAO Cocatalyst

Temp, °C	micromolesZr	Activity	I2	I21	MFR	BBF
85	0.5	30,588	0.839	35.77	42.62	17.38

Mn	Mw	PDI
25,951	161,063	6.21

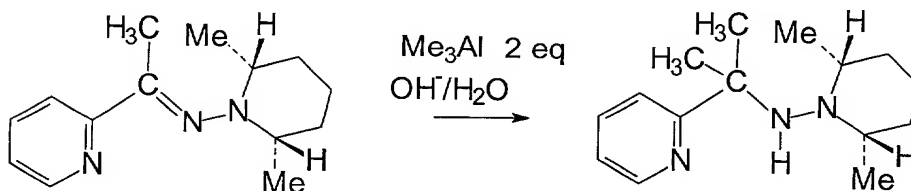
Reaction Conditions: 85°C, 600 mL hexane, 43 mL 1-hexene, MMAO, MMAO/Zr = 1,000.

[00116] Synthesis of 2-Acetylpyridine(1-Amino-cis-2,6-dimethyl piperidine)



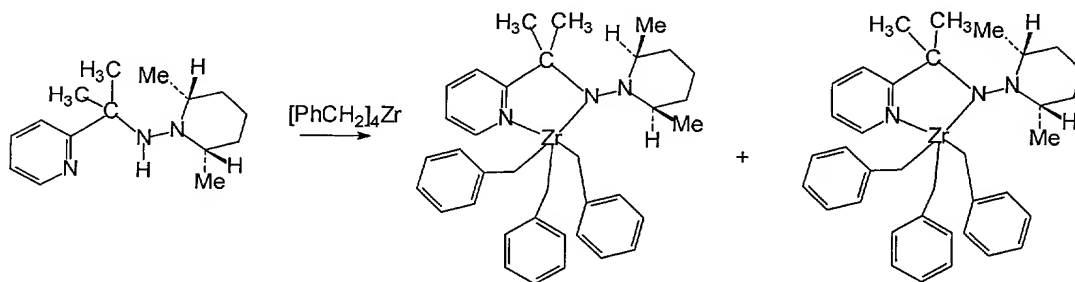
[00117] General procedure: 2-Acetylpyridine (100 mmol, 12.1g) was charged to a 100 mL Schlenk flask equipped with a stir bar and septum. Hydrochloric acid (4.0 mmol, 4.0 mL, {1.0M solution in ether}) was added under a Nitrogen purge. 1-amino-cis-2,6-dimethyl piperidine (80 mmol, 9.9g,) was added to the reaction flask. A Dean-Stark apparatus was attached and the reaction vessel was heated to 105°C while under a nitrogen sweep. After one hour the Dean –Stark apparatus was replaced with a short path distillation head. One fraction was collected from the reaction.

[00118] Alkylation of 2-Acetylpyridine(1-Amino-cis-2,6-dimethyl piperidine)



[00119] General procedure: 2-acetylpyridine(1-amino-cis-2,6-dimethyl piperidine)imine (20 mmol, 4.6g) and 10 mL toluene were charged to a 50 mL Schlenk flask equipped with a stir bar and septum. The reaction vessel was chilled to 0° C. Trimethyl aluminum (63 mmol, 31.5 mL, [2.0M solution in toluene]) was added dropwise. The reaction was allowed to slowly warm to room temperature. When the reaction was complete the solution was transferred into a stirring solution of sodium hydroxide and water, extracted with toluene. The extracts were dried over MgSO₄ and filtered. The filtrate was vacuum stripped to 4g of amber liquid. Analysis by gas chromatography and ¹H NMR in Benzene-d₆ indicated approximate 80% conversion.

[00120] Reaction of the Amine derived from Alkylation of 2-Acetylpyridine(1-Amino-cis-2,6-dimethyl piperidine)imine with Tetrabenzyl zirconium



[00121] General procedure: In dry the box tetrabenzyl zirconium (0.200mmol, 0.091g,) was charged to a 7 mL amber bottle equipped with a stir bar and cap. Benzene-d₆ (1.5 mL) was added and stirred to dissolve. To a vial was charged the Amine derived from alkylation of 2-acetylpyridine(1-amino-cis-2,6-dimethyl piperidine)imine (0.200 mmol, 0.050 g) and 1.5 mL Benzene-d₆. The ligand solution was transferred into the tetrabenzyl zirconium solution. The reaction was allowed to stir at room temperature overnight.

[00122] Polymerization activity with these dimethylcarbon-bridged catalysts was higher than for the corresponding methylbenzylcarbon-bridged catalysts. Comonomer

incorporation was similarly low. Molecular weight again appears to surprisingly decrease at lower zirconium concentrations.

MMAO Cocatalyst, 2.0 micromoles MMAO/Zr = 1,000

Activity	I2	I21	MFR	BBF
45,059	0.132	9.88	74.52	2.55

Conditions: 85°C, 85 psi ethylene, 43 mL hexene, no hydrogen.

MMAO Cocatalyst, 0.5 micromoles MMAO/Zr = 1,000

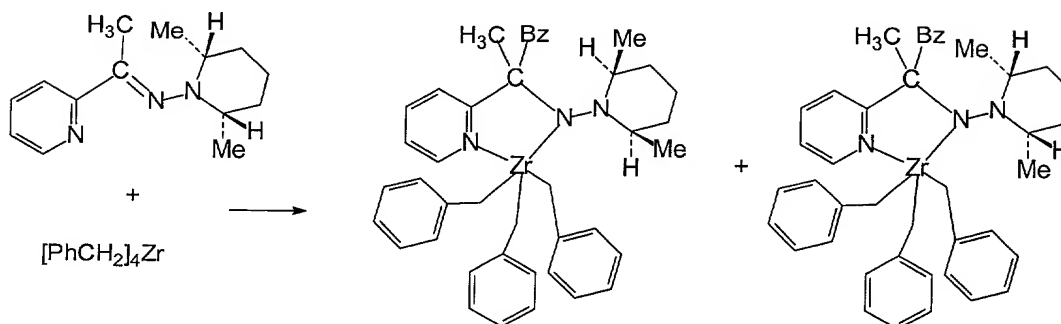
Activity	I2	I21	MFR	BBF
34,353	4.49	111	24.72	3.22

Conditions: 85°C, 85 psi ethylene, 43 mL hexene, no hydrogen.

[00123] Polymerization activity with these dimethylcarbon-bridged catalysts was higher than for the corresponding methylbenzylcarbon-bridged catalysts. Comonomer incorporation was similarly low. Molecular weight again appears to surprisingly decrease at lower zirconium concentrations. One normally encounters lower molecular weights at higher aluminum concentrations due to polymer chain-transfer to aluminum. The results are contrary to that here.

[00124] Size Exclusion Chromatography (SEC) analysis demonstrated that bimodal distributions are possible with this catalyst system. Interestingly, by increasing the zirconium and aluminum concentrations (2.0 micromoles Zr vs 0.5 micromoles Zr and 2,000 micromoles MMAO vs 500 micromoles MMAO) a bimodal distribution was achieved. The results are illustrated in the Figure hereto.

[00125] Reaction of 2-Acetylpyridine(1-Amino-cis-2,6-dimethyl piperidine)imine with Tetrabenzyl zirconium



[00126] General procedure: In dry the box tetrabenzyl zirconium (0.200mmol, 0.091g) was charged to a 7 mL amber bottle equipped with a stir bar and cap. Benzene-d₆ (1.5 mL) was added and stirred to dissolve. To a vial was charged 2-acetylpyridine(1-amino-cis-2,6-dimethyl piperidine)imine (0.200 mmol, 0.046 g) and 1.5 mL Benzene-d₆. The ligand solution was transferred into the tetrabenzyl zirconium solution. The reaction was allowed to stir at room temperature overnight.

Good polymerization activity was observed at 85°C.

MMAO Cocatalyst, 2.0 micromoles MMAO/Zr = 1,000

Activity	I2	I21	MFR	BBF
26,824	1.60	159.0	99.65	2.05

Conditions: 85°C, 85 psi ethylene, 43 mL hexene, no hydrogen.

Good polymerization activity was observed at 85C.

MMAO Cocatalyst, 2.0 micromoles MMAO/Zr = 1,000

Activity	I2	I21	MFR	BBF
26,824	1.60	159.0	99.65	2.05

Conditions: 85°C, 85 psi ethylene, 43 mL hexene, no hydrogen.

[00127] It is noteworthy that this 85°C activity is much higher than for the corresponding 2,5-dimethylpyrrole-amide complex documented earlier. The 2,6-dimethylpiperidine derivative apparently has better thermal stability than this system. Polymerizations using 0.5 micromoles of zirconium complex at various temperatures.

MMAO Cocatalyst, 0.5 micromoles MMAO/Zr = 1,000

T, °C	Activity	I2	I21	MFR	BBF
85	19294	87.43	20K	229	3.00
85	18,353	27.79	167	6.02	4.06
85	19,294	21.95	103	4.69	2.74
75	18,824	1.94	47.03	24.28	2.88
95	7,059	-	-	-	-
105	2,353	-	-	-	-

Conditions: 85°C, 85 psi ethylene, 43 mL hexene, no hydrogen.

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